

REINHOLD ENVIRONMENTAL Ltd.



**2018 NO<sub>x</sub>-Combustion Round Table  
& Expo Presentation**

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# Economic Advantages of Strategic SCR Catalyst Cleaning and Management

Presented by Michael Ware II / President SCR Solutions, Inc.

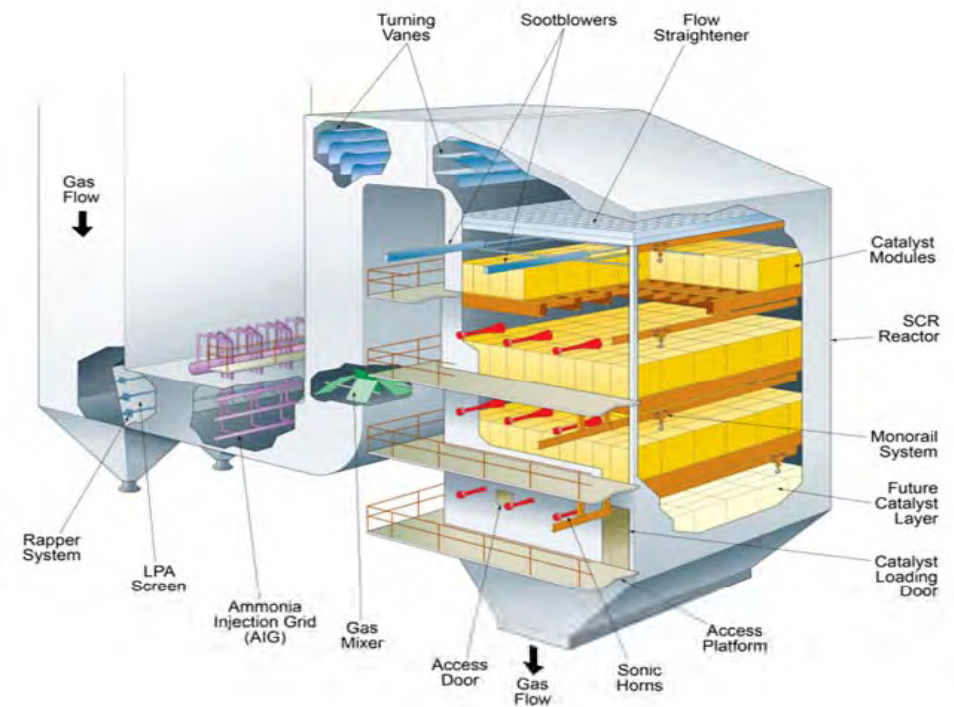
SCR Consultant for:  
**Thompson Industrial Services, LLC**

**2018 NOX-COMBUSTION-CCR/PCUG  
CONFERENCE**



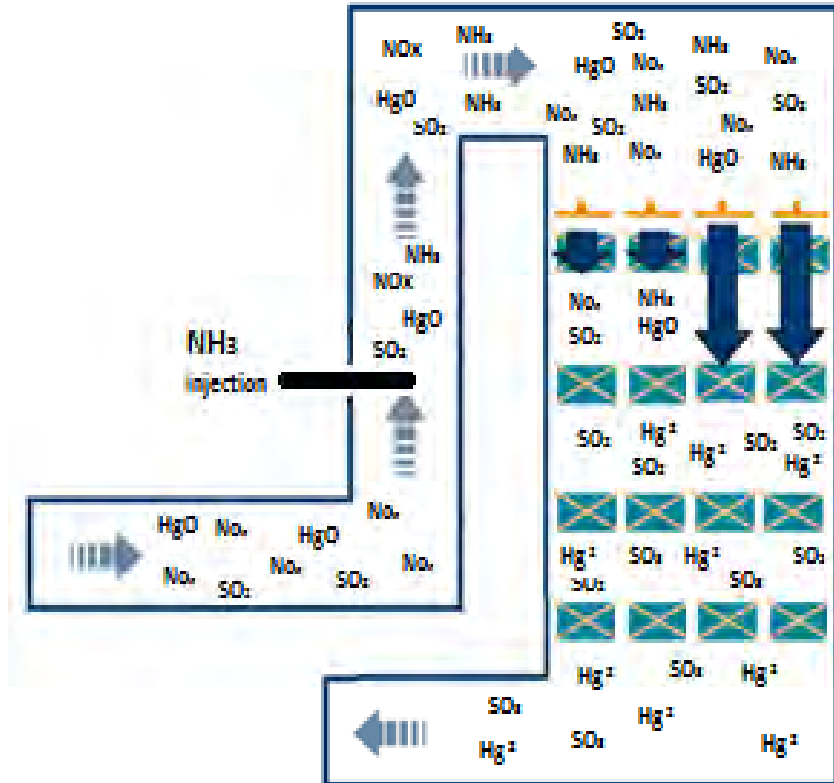
# Requirements for Optimal SCR Efficiency

- **Even Flow & Distribution**
- **Proper Ammonia-to-NOx Balance**
- **Maximum Catalyst Surface Area for NOx & Mercury Oxidation**



# Need for Maximum Catalyst Surface Area

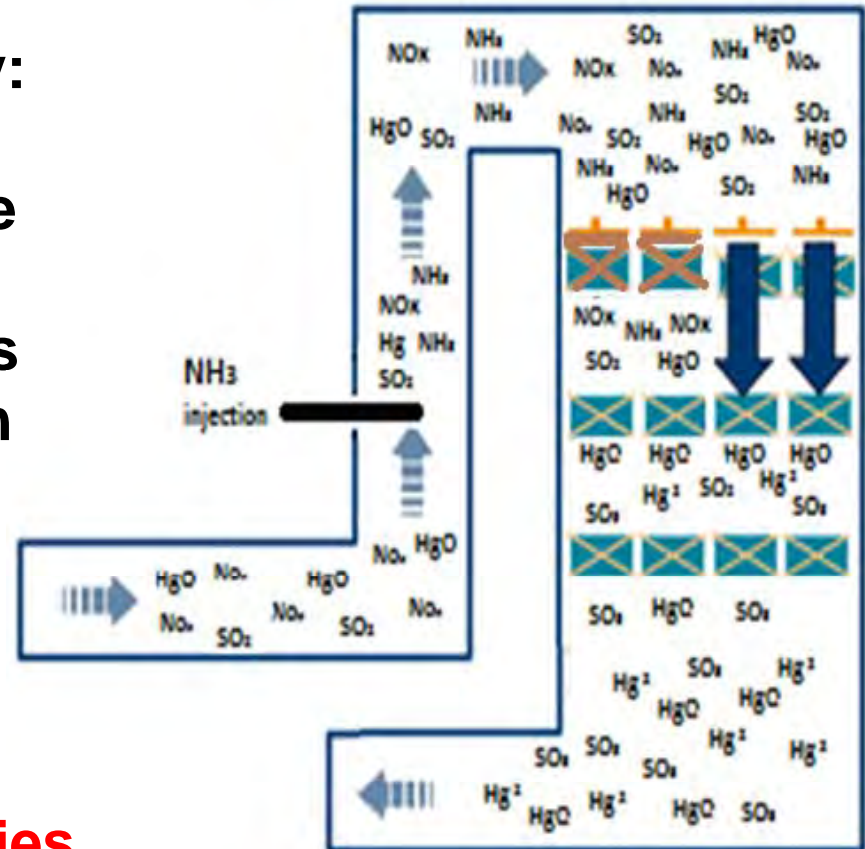
- **Flue Gas Stream Contains:**
  - Nitrogen Oxides
  - Sulfur Dioxide
  - Mercury
- **NO<sub>x</sub> competes for Oxygen and wins over both Sulfur Dioxide and Mercury.**
- **The presence of ammonia inhibits Mercury and Sulfur Dioxide conversion.**



# Catalyst Life

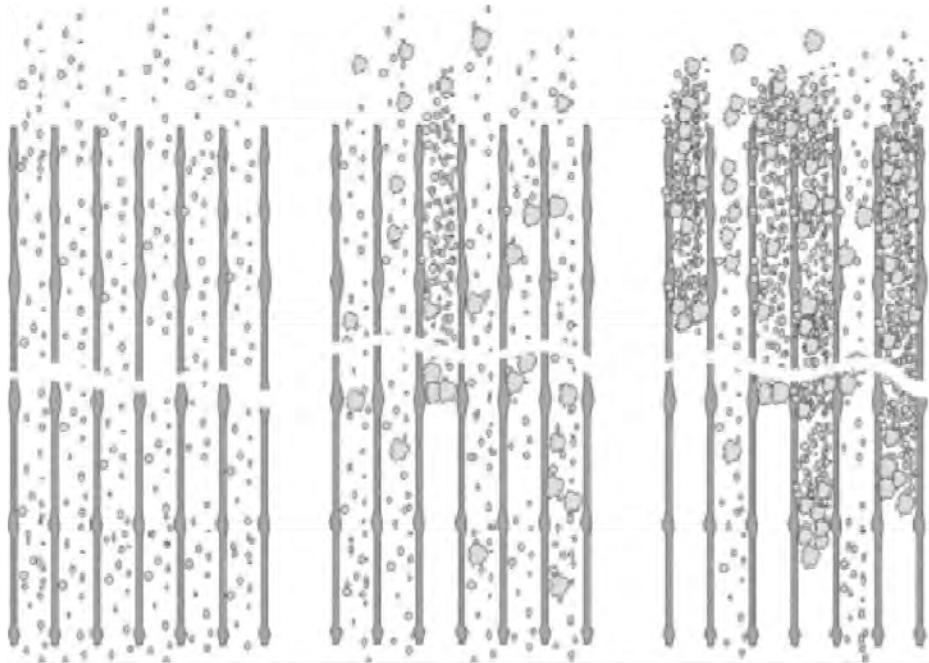
Catalyst deactivation is caused by:

- Poisoning of active sites by flue gas constituents
- Thermal sintering of active sites due to high temperatures within reactor
- **Blinding/plugging/fouling of active sites by ammonia-sulfur salts and particulate matter.**
- **Erosion due to high gas velocities.**



*As the catalyst activity decreases,  $\text{NO}_x$  removal decreases & ammonia slip increases.*

# Vacuuming



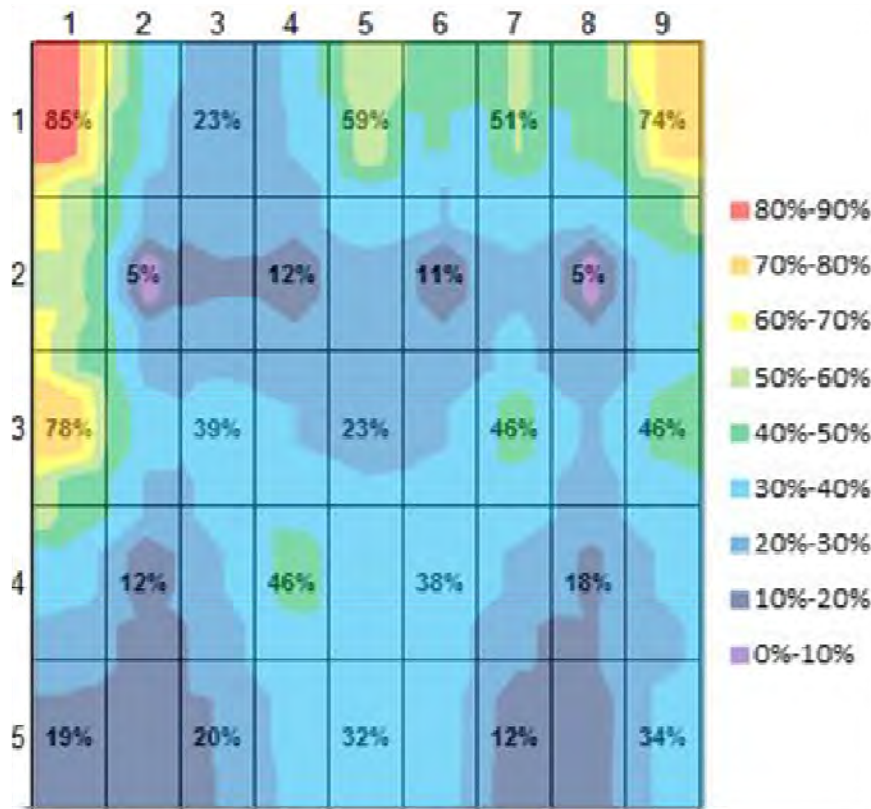
**Simply vacuuming the fly ash off the top of the catalyst screens and catalyst surface does not effectively clear the inner catalyst surface or pores from physical or chemical poisoning substances.**

# Vibration Cleaning in Action

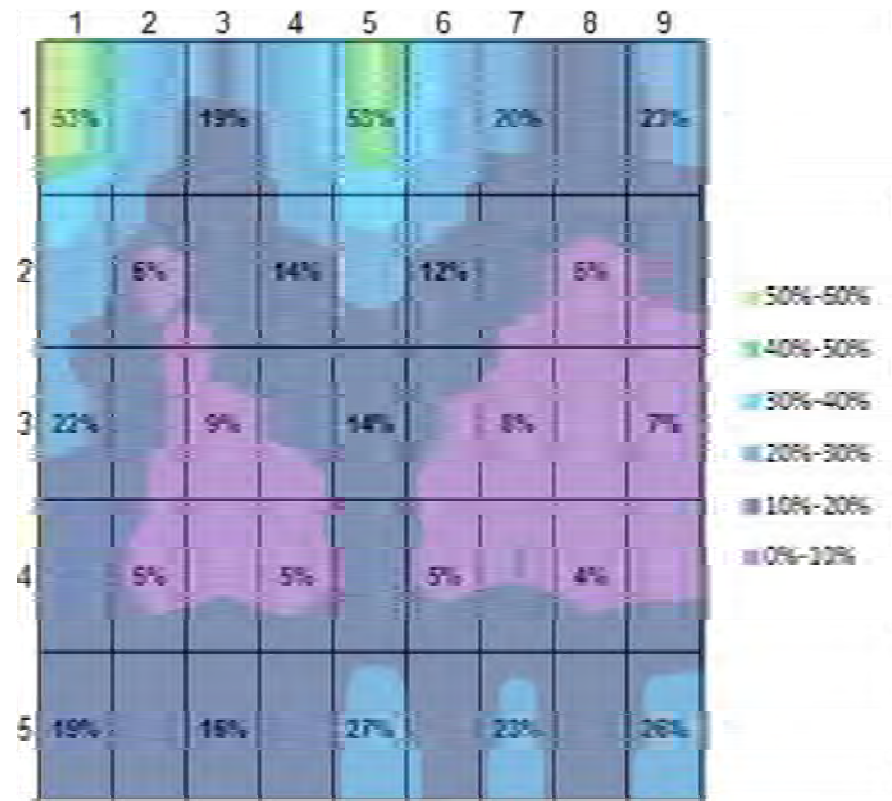


# Traditional vs. Vibration Technology

## Traditional Cleaning



## Vibration Cleaning Results



## Removal of Hardened Ash

***Sponge Blasting Process*** utilizes polyurethane foam media to **Safely Remove Hardened Ash from the Surface and Within the Catalyst without Damage.**



# Sponge Blasting in Action

## Sponge Blasting for Unplugging & Removal of Hardened Ash

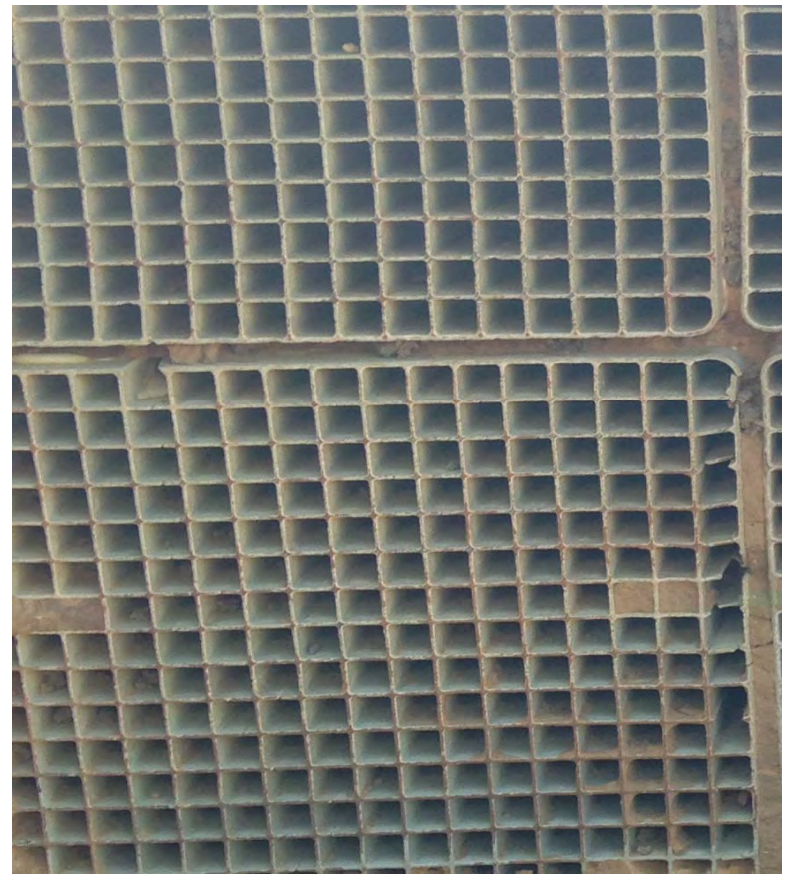


# Results

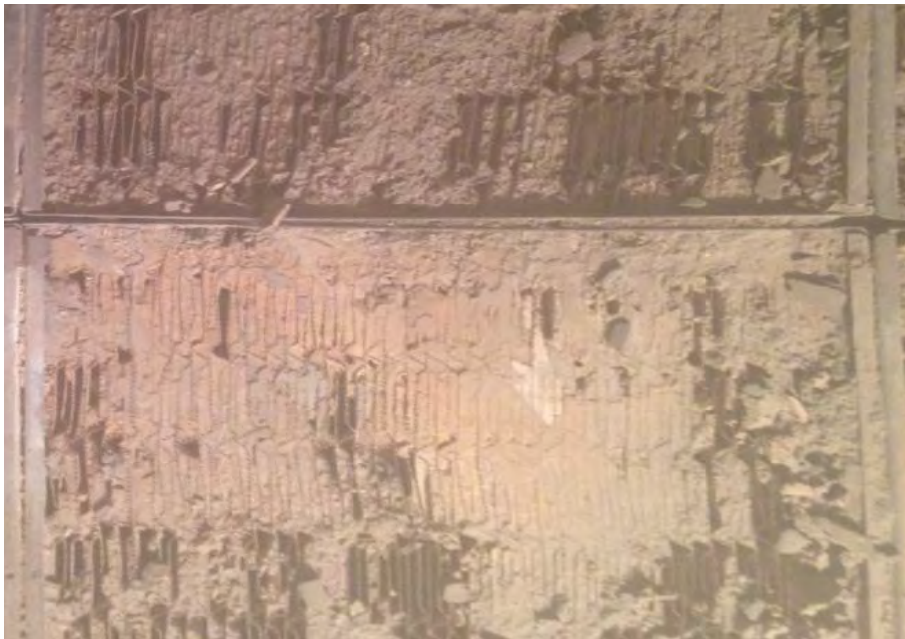
**BEFORE**



**AFTER**



# Results



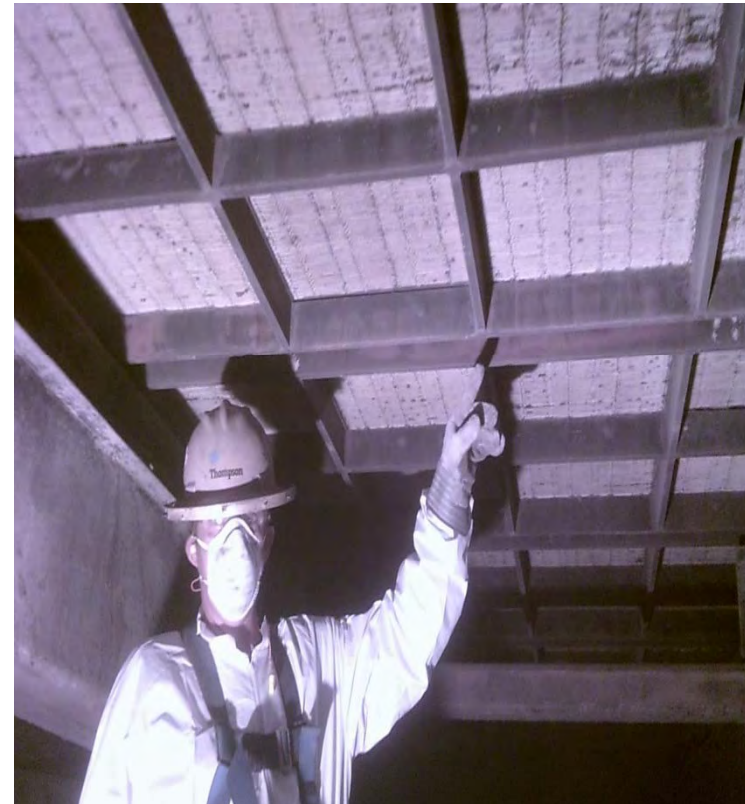
This combination of methods **Safely Clears both honeycomb and plate Catalyst of Potentially Harmful Contaminates that cannot be achieved by traditional methods.**

# Bottom of Catalyst Layer

**Before In-situ Cleaning Process**



**After In-situ Cleaning Process**



## Cost of Reduction in Catalyst Activity

LAYER	INVESTMENT	LOSS AT 25%	REMAINING VALUE
1	\$1,000,000	\$250,000	\$750,000
2	\$1,000,000	\$250,000	\$750,000
3	\$1,000,000	\$250,000	\$750,000
<b>Total</b>	<b>\$3,000,000</b>	<b>\$750,000</b>	<b>\$2,250,000</b>

***\*Cost averaged between New Catalyst at \$1,200,000 and Regenerated Catalyst at \$800,000 (based on 192 Modules Per-Layer with 25% Loss Over 18-Month Outage Cycle). Does Not Include Cost of Installation.***

# Traditional Cleaning vs Advanced Cleaning Technologies

Layer	Cost	Cost of 25% Pluggage	Traditional Cleaning	Total	5 % Recovered	Loss Per-Outage Cycle
1	1 Mill.	250k	20k	270k	50k	220k
2	1 Mill.	250k	20k	270k	50k	220k
3	1 Mill.	250k	20k	270k	50k	220k
<b>Total</b>	<b>3 Mill.</b>	<b>750k</b>	<b>60k</b>	<b>810k</b>	<b>150k</b>	<b>660k</b>
Layer	Cost	Cost of 25% Pluggage	Advanced Technologies	Total	15 % Recovered	Loss Per-Outage Cycle
1	1 Mill.	250k	40k	290k	150k	140k
2	1 Mill.	250k	40k	290k	150k	140k
3	1 Mill.	250k	40k	290k	150k	140k
<b>Total</b>	<b>3 Mill.</b>	<b>750k</b>	<b>120k</b>	<b>870k</b>	<b>450k</b>	<b>420K</b>
					<b>NET GAIN</b>	<b>\$240,000.00</b>

*\*As pluggage percentage continues to compound, (80% vs 90%), erosion will increase more rapidly.*

# Value of Extending Catalyst Life

Layer	Cost	Installation	Traditional	Invested
1	1 Mill.	400k	60k	1,460,000.00
2	1 Mill.	400k	60k	1,460,000.00
3	1 Mill.	400k	60k	1,460,000.00
Total	3 Mill.	1.2 Mill.	180k	4,380,000.00
			18 Mo. x3	54 Months
			Per Month	\$81,111.11

Layer	Cost	Installation	Advanced	Invested
1	1 Mill.	400k	120k	1,520,000.00
2	1 Mill.	400k	120k	1,520,000.00
3	1 Mill.	400k	120k	1,520,000.00
Total	3 Mill.	1.2 Mill.	360k	4,560,000.00
			24 Mo. x3	72 Months
			Per Month	\$63,333.33

## Costly Effects of Pluggage

- **Reduction in Catalyst Life**
  - **Decreased Catalyst Efficiency**
  - **More Frequent Catalyst Replacement**
  - **Increased Pressure Drop Across the SCR**
  - **Increased Fan Power Consumption**
  - **Reduced Efficiency of Mercury Removal**
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# Costly Effects of Pluggage

- **Poor Ammonia Distribution**
- **Ammonia Slip**
- **Increase Regent Usage**
- **Formation of Ammonium Bisulfate (ABS) in the Air Preheater.**

**Increased air preheater fouling.**

**Increased back end corrosion**

- **Interrupted Power Production & Revenues**

# SCR Management Options

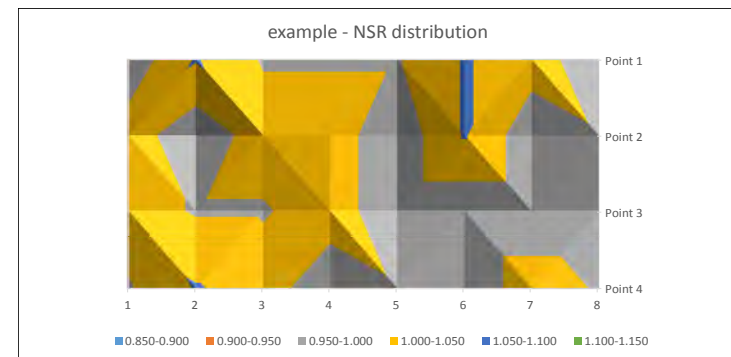
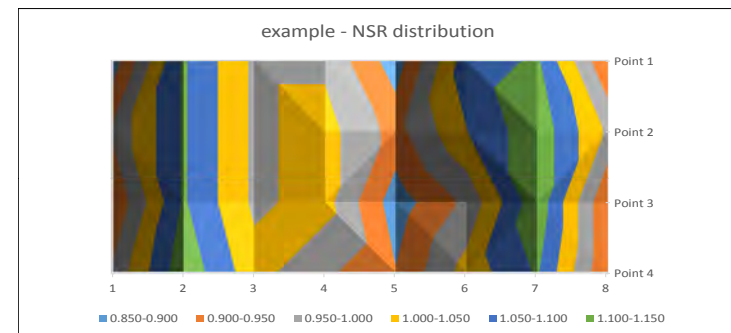
- **Catalyst cleaning alone cannot solve all SCR related issues.**
- **Other tools to troubleshoot SCR issues and optimize system operation**
  - Boiler tuning
  - SCR tuning
  - Bench-scale SCR catalyst testing

# Boiler Tuning

- **Visual inspection of burners, air and gas systems, and pulverizers**
- **Controls evaluation during unit swing/ramp**
- **Validation of airflow indications**
- **Baseline testing from to evaluate**
  - $\text{NO}_x/\text{CO}/\text{O}_2$  distribution within furnace
  - Fuel fineness/distribution and air-to-fuel ratio
  - Air in-leakage
- **Tuning operating parameters to optimize unit efficiency and minimize emissions**
  - Reduced furnace exit  $\text{NO}_x$  and LOI
  - Improved heat rate

# SCR Tuning

1. Inspect ammonia injection nozzles, if possible
2. Document inlet  $\text{NO}_x$  distribution/AIG injection valve position
3. Tune  $\text{NH}_3$  injection to meet  $\text{NO}_x$  distribution
4. Retest SCR inlet/outlet  $\text{NO}_x$  until desired result achieved



# SCR/Boiler Tuning: Economics

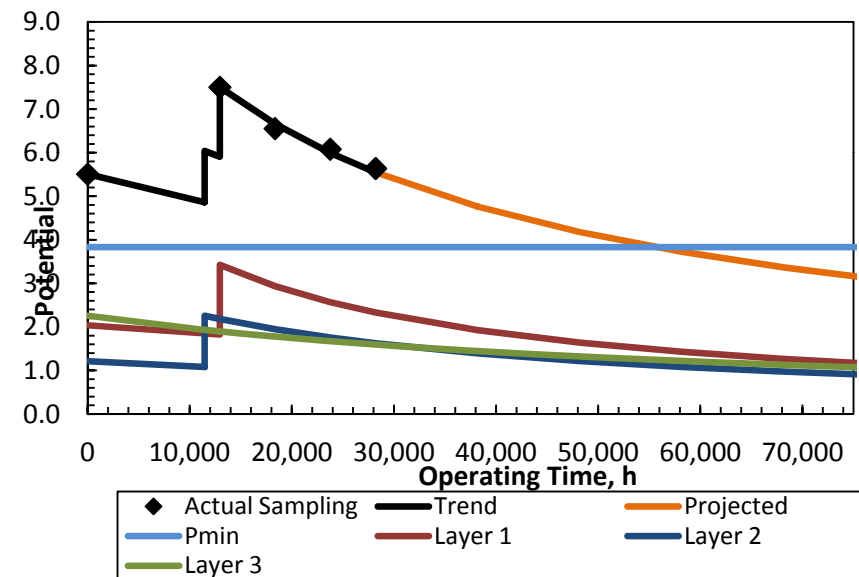
- Reduction in boiler exit  $\text{NO}_x$  can pay for cost of tuning program in one year
  - Reduced  $\text{NH}_3$  consumption
- Additional benefits
  - Improved heat rate
  - Reduced slagging potential
  - Fewer forced outages
- Tuning  $\text{NH}_3$  injection leads to optimal reagent consumption
  - Less  $\text{NH}_3$  slip
  - Balanced distribution

*Annual  $\text{NH}_3$  Savings for Given Boiler Exit  $\text{NO}_x$  Reduction/ $\text{NH}_3$ : $\text{NO}_x$  Distribution Improvement (600 MW Unit)*

	2%	5%	10%
PRB	\$19,800	\$49,400	\$98,800
Illinois Basin	\$25,400	\$63,500	\$127,000
Bituminous	\$32,500	\$81,100	\$162,300

# SCR Catalyst Testing

- Track catalyst deactivation trends
- Determine primary catalyst deactivation mechanisms
- Project catalyst lifetime
- Optimize catalyst replacement schedules
- Evaluate impact of changing fuel type



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**Presented by: Michael Ware II**

*President ,SCR Solutions, Inc.*

*SCR Consultant for Thompson Industrial Services, LLC*

# Questions?



**Thompson**  
Industrial Services